



TECHNICAL SEMINAR on Onboard  
Carbon Capture and Storage(OCCS) Systems

# Developing Total Solutions for OCCS

Insights from “Real-Ship Projects” in Safety, Operation, and Regulation

PRESENTED BY  

September 1<sup>st</sup>, 2025

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# 01

Chapter

## Introduction

- Why OCCS, its Opportunities and Challenges

## OCCS is an immediate solution to achieve Net Zero by 2050

- 1 To adopt OCCS to vessels to meet Net Zero by 2050, especially for existing fleets is inevitable
- 2 However, in the process of applying it to actual ships, there are various technical, operational, and regulatory hurdles.

### Safety

- Large CO<sub>2</sub> storage in non-gas carrier
- Amine
- Refrigerant

### Training

- Unfamiliar to seafarers
- Assistance from shore-based experts is required.

### Value chain

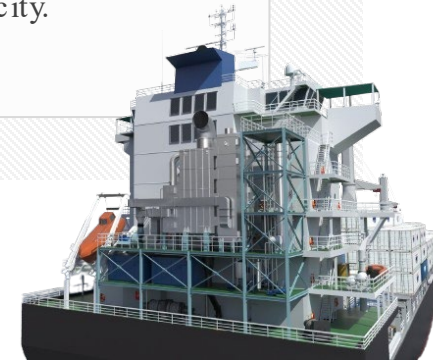
- No experience for unloading and utilization.

### Efficiency

- Energy is consumed during carbon capture and liquefaction.

### Space

- Equipment consumes space and adds weight, resulting in a reduction of cargo capacity.





# 02

Chapter

## Real-Ship Application Overview

- Brief on real-ship demonstration consortium  
: Korean Register, PANASIA, Samsung Heavy Industries, HMM
- Vessel Information
- OCCS Flow Diagram & Specification

## Consortium for Onboard Carbon Capture System

Teaming up to reduce the GHG in short term



Classification

### Survey & Research

- Drawing approval
- Risk assessment
- Safety rule development

### Container Ship Operation

- Ship owner
- Captured CO<sub>2</sub> unloading



Ship Owner



Equipment Maker

### OCCS Supplier & Retrofit

- Carbon capture system supplier
- Retrofit engineering

### Liquefaction Facility

- Liquefaction system supplier
- Captured CO<sub>2</sub> utilizing

SAMSUNG

Ship Builder

## Fundamental Design check-up points



### SHIP'S PARTICULAR

Vessel Name / Flag	HMM MONGLA / J E J U, KOREA
Vessel Type	Container Vessel
Vessel Capacity	2,200 TEU
Fuel Type	HFO ( With SO <sub>x</sub> -Scrubber)
1-Cycle Voyage Period	270 days voyage/year
Fuel Consumption	29.7ton per day
Vessel CO <sub>2</sub> Emission Per Year	24,977 Ton.CO <sub>2</sub> /year

Item	Spec.
Electrical power	6650 kW
Composite boiler	1.6t(Exh.) / 1.8t(O.F)
F.W Gen.	25 t/day

# OCCS Flow Diagram & Specification

## 1 Pre-treatment of Flue Gas

Flue gas is cooled, and particles and sulfur oxides are removed. It is then pressurized and sent to the absorber.

## 2 CO<sub>2</sub> Absorption

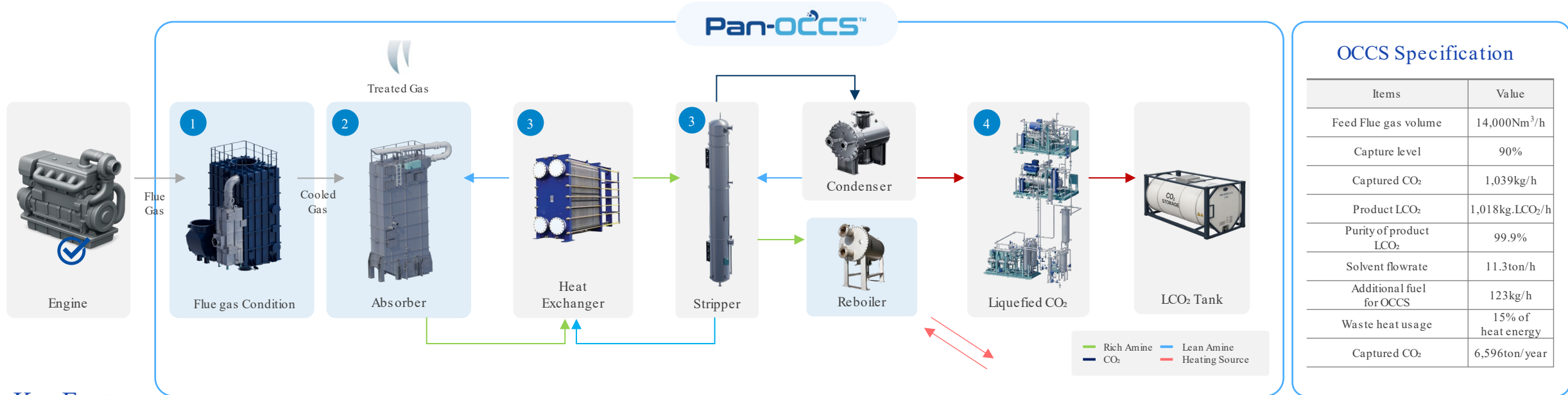
The cooled gas contacts a chemical solvent in the absorber, selectively capturing CO<sub>2</sub>.

## 3 Regeneration

The solvent is heated by a reboiler to release the captured CO<sub>2</sub> and regenerate it for reuse.

## 4 Liquefaction & Storage

CO<sub>2</sub> is liquefied through compression and cooling, allowing safe marine storage and efficient onshore off-loading.



## Key Features

✓ Combined functions of Scrubber and OCCS

✓ Optimized Space utilization

✓ Improved energy efficiency



# 03

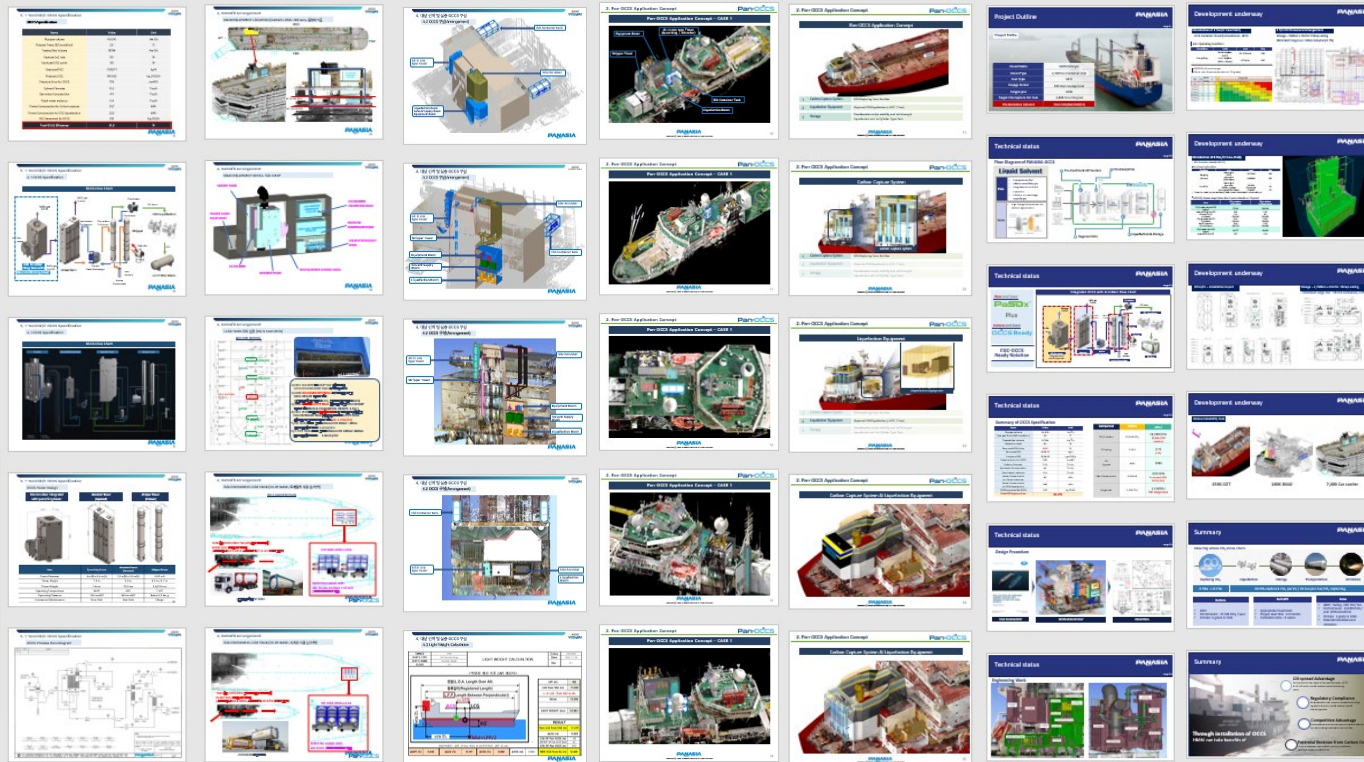
Chapter

## Design Optimization and Efficiency Considerations

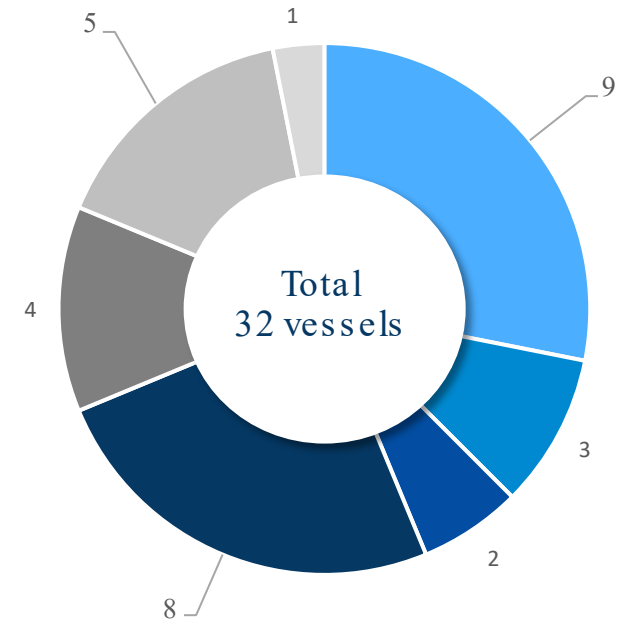
- Feasibility Study
- Technical Challenges
  - OCCS Optimization – Space & Energy
  - LCO<sub>2</sub> storage design
  - Supporting Crews
- Voyage Summary of HMM MONGLA during Past 1 Year
- Offloading LCO<sub>2</sub>

# Feasibility Study 1 Successfully Completed

The system has been applied to various vessel types, including bulk carriers, tankers, and gas carriers, with supported capacities ranging from 0.5 to 8 tons per hour.

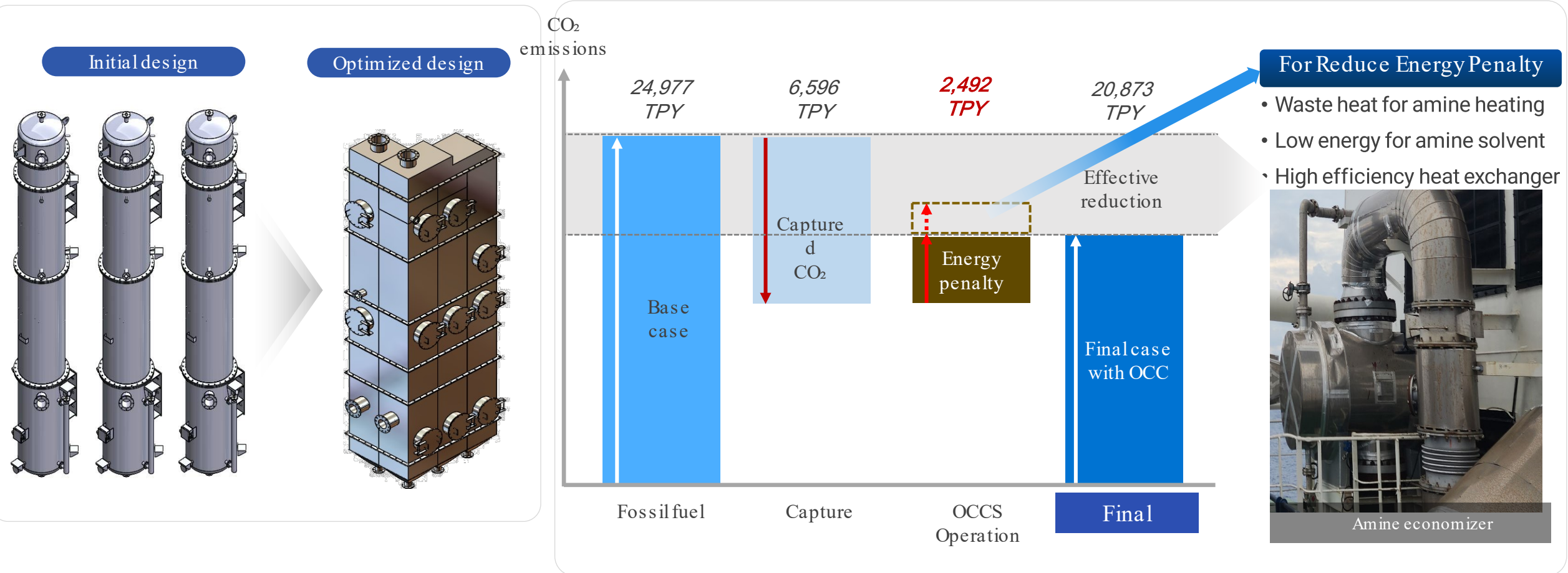


■ CNTR. ■ LNGC ■ PCTC ■ B.C ■ C.O.T ■ P.C ■ Other



# 1. Technical Challenges I OCCS Optimization – Space & Energy

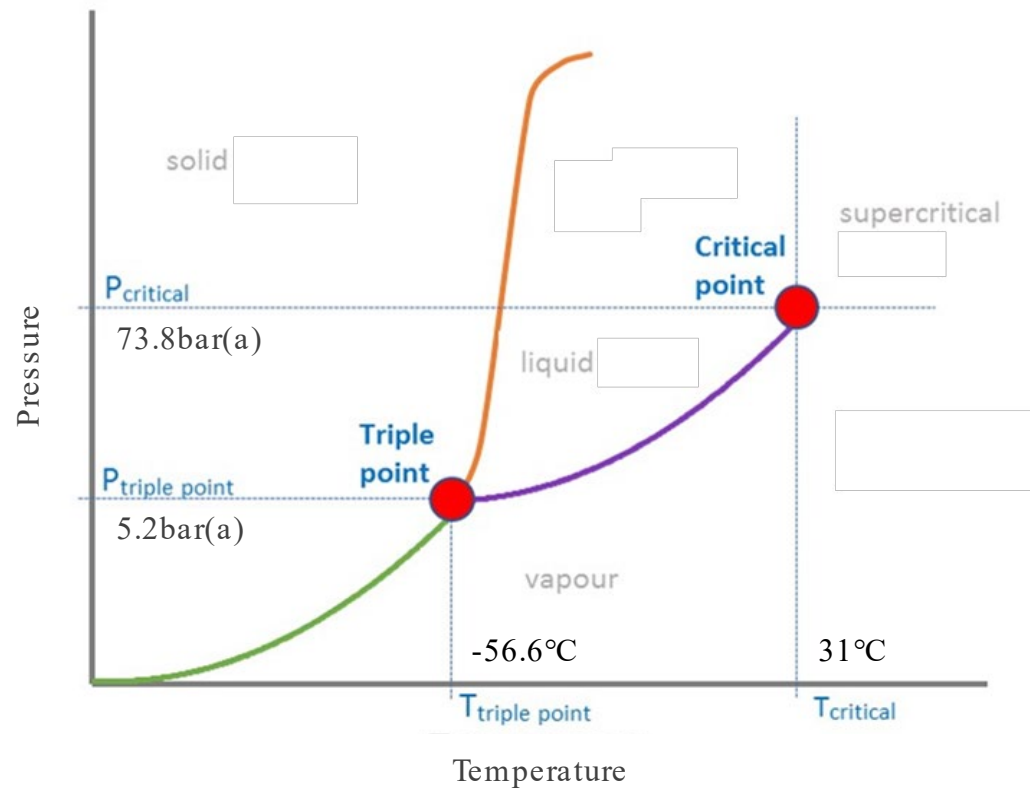
Adding OCCS into optimized designed vessel is a challenge.  
However, one tower solution and Reboiler for Amine delivers a Optimized solution in efficiency



## 2. Technical Challenges I LCO<sub>2</sub> storage design

Design of LCO<sub>2</sub> Storage is various and requires the common standard

Triple point and Critical point

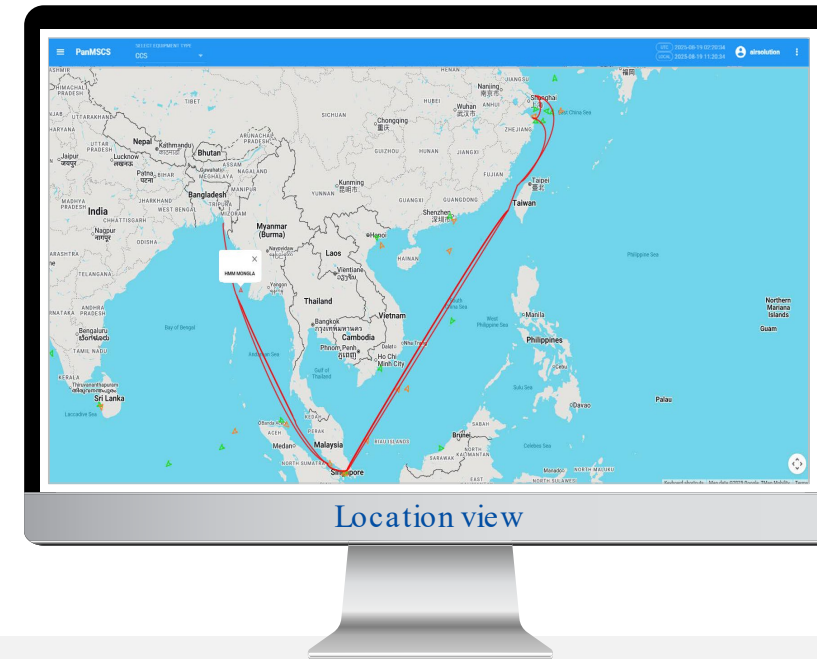
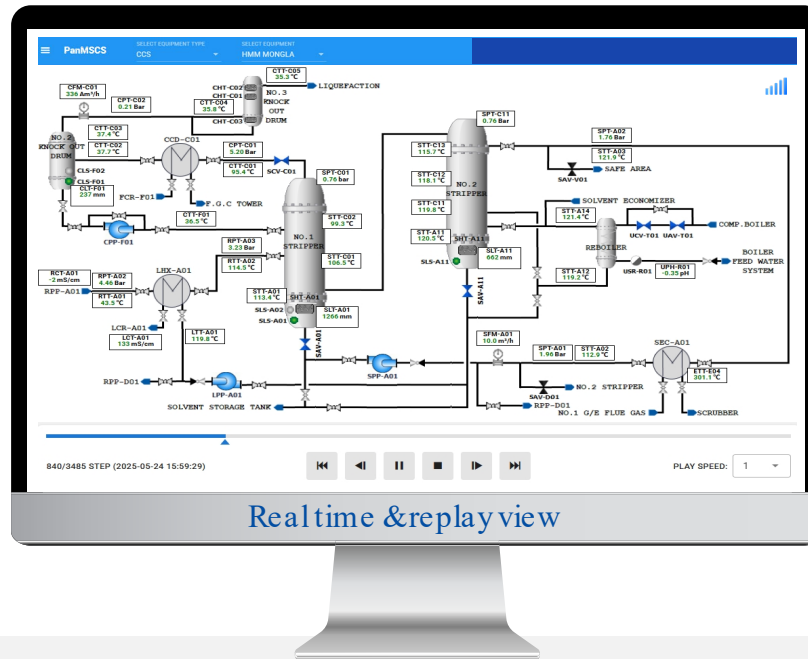


	Low Pressure	Conventional	Unit
Pressure	7 ~ 8	15 ~ 20	bar(a)
Boiling Temperature	-49 ~ -46	-29 ~ -20	°C
Density	1152 ~ 1140	1070 ~ 1029	kg/m <sup>3</sup>
Storage Efficiency	High	Low	
Dry Ice Possibility	High	Low	
Tank Cost	Low	High	



### 3. Technical Challenges I Supporting Crews

Real-ship OCCS project was designed not only perform its functionality but beyond through on-line support



☑ Minimize extra work for crews

new system to crews can cause extra workload to operate

☑ Safety of crews and ships

simultaneously monitor the system from the ship and manufacturer.

☑ Providing a guide

Immediate support can be provided when necessary.

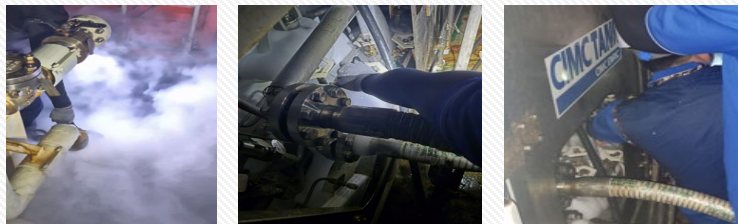


# Voyage Summary of HMM MONGLA during Past 1 Year

Liquefaction Set-up



Flexible Line Purging & Valve Arrange



HMM Safety Check





# Voyage Summary of HMM MONGLA during Past 1 Year


LCO<sub>2</sub> offloaded at the port and brought to produce Green Methanol



No.	Date	Route	Detail Performance
1	Jul 12 – Aug 4, 2024	MOK – NGB – SHA – CGP	Initial setup, installation inspection
2	Sep 12 – Oct 19, 2024	SIN – NGB CGP – PKL – SIN	Testing capture system
3	Oct 19 – Nov 22, 2024	SIN – NGB CGP – SING	Testing liquefaction system
4	Nov 22 – Nov 30, 2024	SIN – NGB	Operating full OCCS and LCO <sub>2</sub> storage
5	Dec 31, 2024 – Jan 6, 2025	SIN – NGB	<b>Off-loading (17/16Ton)</b>
6	Feb 1 – Feb 9, 2025	SIN – NGB	OCCS Notation
7	Apr 16 – Apr 24, 2025	SIN – NGB	Operating full OCCS and LCO <sub>2</sub> storage
8	May 19 – May 25, 2025	SIN – NGB	<b>Off-loading (15/10Ton)</b>
9	Jul 22 – Jul 3, 2025	SIN – NGB	Maintenance

Real-ship results, optimized design, and regulatory compliance combine to complete the total solution.

PROPERTY	METHOD	RESULT UNITS	MIN	MIX
Carbon Dioxide	GB/T 1886.228-2016	> 99.9% (V/V)	--	-
Water by Dew Point	GB/ 7 5832.2-2016	2.14ppm (v/v)	-	-



Client : SINOTECH CCS CO.,LTD  
Report No. : COPCSH2500133-01B2  
Date of Iss. : 13-Jan-2025 To: 13-Jan-2025  
Client's Ref. : N/A  
Vessel : N/A  
Cargo : Carbon dioxide  
Location : Ningbo, China  
Date of Report : 13-Jan-2025  
Page No. : 2


**SAMPLING REPORT**

Sampling Method: ASTM D1265-23a

DATE	SAMPLE DESCRIPTION			CONTAINERS		SAMPLE TYPE	SEAL NO. (SGS-OGC)
	STATUS	SOURCE	PURPOSE	QTY	Type		
13-Jan-2025	-	CICU3881767	Analysis	2*1L	Cylinders	Tap	-
13-Jan-2025	-	CICU3881767	Analysis	1*3L	Vapor bags	Tap	-

Weather condition during sampling:  
☒ Normal  
☐ Abnormal weather condition: \_\_\_\_\_

Unless otherwise instructed, the above samples will be retained only for \_\_\_\_\_



Authorized Signature  
SGS (Shanghai) Technical Services (Shanghai) Co., Ltd.

	METHOD	RESULT UNITS	MIN	MAX
Carbon Dioxide	GB/T 1886.228-2016	>99.9 % (V/V)	--	--
Water by Dew Point	GB/T 5832.2-2016	2.14 ppm (v/v)	--	--
Hydrogen Sulfide	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Sulfur Dioxide	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Methanethiol	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Ethanethiol	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
2-Propanethiol	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Carbonyl Sulfide	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Dimethylsulfide	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Diethylsulfide	ASTM D5504-20	<0.1 mg/m <sup>3</sup>	--	--
Total Sulfur	ASTM D5504-20	<1 mg/m <sup>3</sup>	--	--
Ammonia as NH <sub>3</sub>	HJ 535-2009	<1 mg/m <sup>3</sup>	--	--
Formaldehyde Content	HJ 601-2011	<1 mg/m <sup>3</sup>	--	--
Acetaldehyde	ASTM D7423-23	<1 mg/kg	--	--
Hydrogen	GB/T 9722-2023	<50 ppm (v/v)	--	--
Nitrogen	GB/T 9722-2023	<0.01 % (V/V)	--	--
Carbon monoxide	GB/T 9722-2023	<0.01 % (V/V)	--	--
Oxygen	GB/T 9722-2023	<10 ppm (v/v)	--	--
Mercury Content	EPA 7473-2007	<100 ng/m <sup>3</sup>	--	--
NOX ( NO+NO <sub>2</sub> )	ASTM D4599-21	11.6 mL/m <sup>3</sup>	--	--

End of Analytical Results



GreenMEOH

Declaration of CO<sub>2</sub> Utilization

二氧化碳利用声明

I. Purpose of CO<sub>2</sub> Utilization 二氧化碳利用目的  
CO<sub>2</sub> is an essential raw material in our methanol production process. By incorporating CO<sub>2</sub> into our manufacturing operations, we aim to not only produce high-quality methanol but also contribute to the reduction of greenhouse gas emissions through a circular economy approach.

二氧化碳是甲醇生产过程中的关键原材料。通过将二氧化碳纳入我们的生产运营，我们不仅旨在生产高质量的甲醇，还希望通过循环经济模式为减少温室气体排放做出贡献。

II. Source of CO<sub>2</sub> 二氧化碳来源  
The CO<sub>2</sub> utilized by GreenMEOH is sourced from the Onboard Carbon Capture System with purity over 99.9% (v/v), which is reliable and compliant with all relevant environmental and safety regulations.

本次合作醇美科技使用的二氧化碳来自船舶碳捕集系统，该来源可靠且符合所有相关的环境和安全法规。

III. Utilization Amount of CO<sub>2</sub> 二氧化碳利用量  
● 1<sup>st</sup> Offloading: 32.2 tons 第一次泄放: 32.2 吨  
● 2<sup>nd</sup> Offloading: 24.1 tons 第二次泄放: 24.1 吨  
Note: The on-site records of the weighing and measurement are provided in the appendix.

注：过磅称量现场记录见附录。

IV. Production Process 生产工艺  
The methanol production process of GreenMEOH involves the reaction of CO<sub>2</sub> with hydrogen (H<sub>2</sub>) under specific temperature, pressure, and catalyst conditions. The chemical reaction can be simplified as follows: CO<sub>2</sub>+3H<sub>2</sub>→CH<sub>3</sub>OH+H<sub>2</sub>O. This process is carried out in a state-of-the-art production facility, ensuring optimal conversion rates and product quality.

醇美科技的甲醇生产工艺是在特定的温度、压力和催化剂条件下，使二氧化碳与氢气发生反应。化学反应可简化如下：CO<sub>2</sub>+3H<sub>2</sub>→CH<sub>3</sub>OH+H<sub>2</sub>O。该工艺在先进的生产设施中进行，确保了最佳的转化率和产品质量。

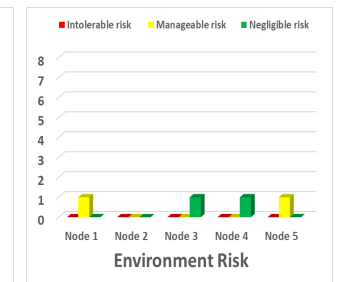
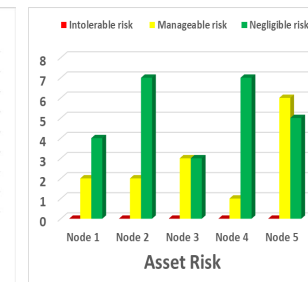
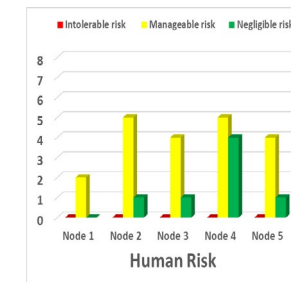
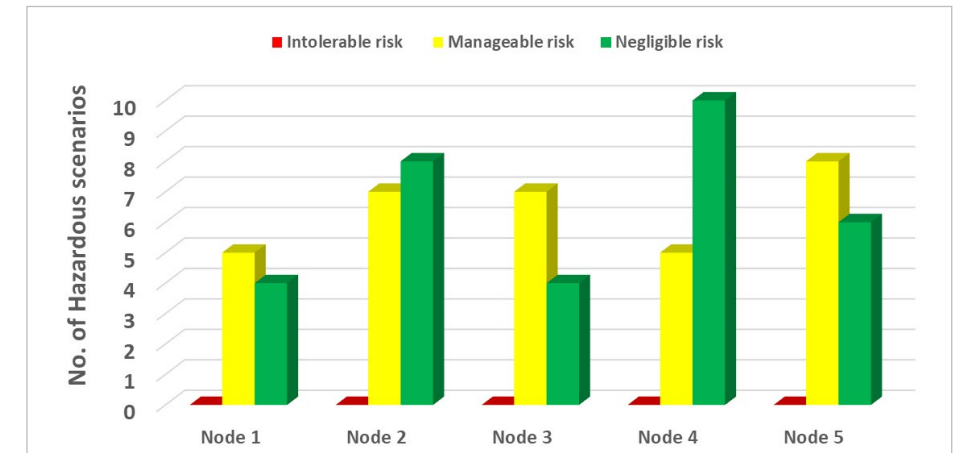
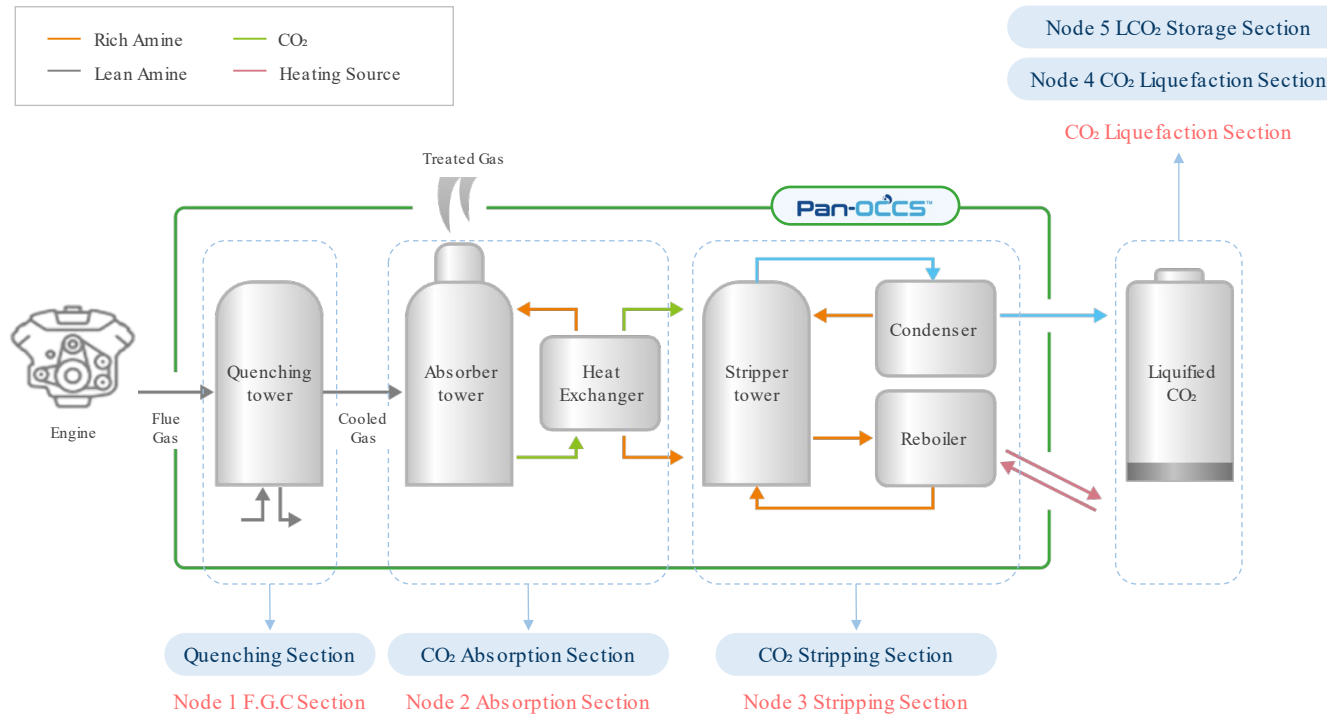
# 04

Chapter

## Regulatory Gaps and Class Experience

- Regulatory Gaps and Class Experience

## HAZID STUDY





## Regulatory Gaps and Class Experience

## HAZID STUDY - Identifying 5 major issues among 252 issues

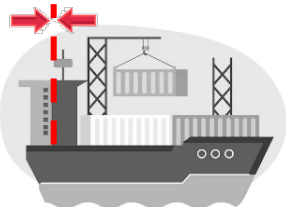
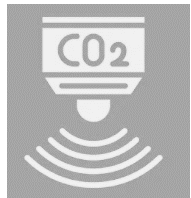
Category	Identified Issue	Measures
Solvent	Leakage	<ul style="list-style-type: none"> <li>- Use of class II pipes with appropriate material</li> <li>- Installation of drip tray liquid detector</li> <li>- Forced ventilation fan in handling space</li> <li>- ESD valve for solvent storage area</li> </ul>
	Freezing	<ul style="list-style-type: none"> <li>- Drain lines for winter season</li> <li>- Heater in solvent storage area</li> </ul>
	Personal Accident	<ul style="list-style-type: none"> <li>- Personal protective equipment (PPE)</li> <li>- Emergency shower and eyewash</li> </ul>
CO <sub>2</sub>	Leakage	<ul style="list-style-type: none"> <li>- Forced ventilation fan in handling space</li> <li>- CO<sub>2</sub> detector</li> <li>- Installation of vent mast</li> </ul>
	Engine Room Ingress	<ul style="list-style-type: none"> <li>- Separated area from engine room and accommodation</li> </ul>
	Freezing	<ul style="list-style-type: none"> <li>- Pressure control logic and alarm</li> <li>- Set-up procedure for tank connection</li> </ul>
	Over-Pressure	<ul style="list-style-type: none"> <li>- Maximum storage day calculation for BOG</li> </ul>
Refrigerant	Leakage	<ul style="list-style-type: none"> <li>- Forced ventilation fan in handling space</li> <li>- Refrigerant detector</li> </ul>
Fire	Solvent	<ul style="list-style-type: none"> <li>- Fire extinguisher (Non-flammability)</li> </ul>
	Equipment	<ul style="list-style-type: none"> <li>- Install fire detectors</li> </ul>
	Refrigerant	<ul style="list-style-type: none"> <li>- Install fixed fire extinguishing system and extinguisher</li> </ul>
	Tank	<ul style="list-style-type: none"> <li>- Water spray for CO<sub>2</sub> tank</li> </ul>
Fresh Water Consumption	F.W Shortage	<ul style="list-style-type: none"> <li>- Apply additional fresh water generator</li> </ul>

HAZID STUDY - CO<sub>2</sub> Leakage

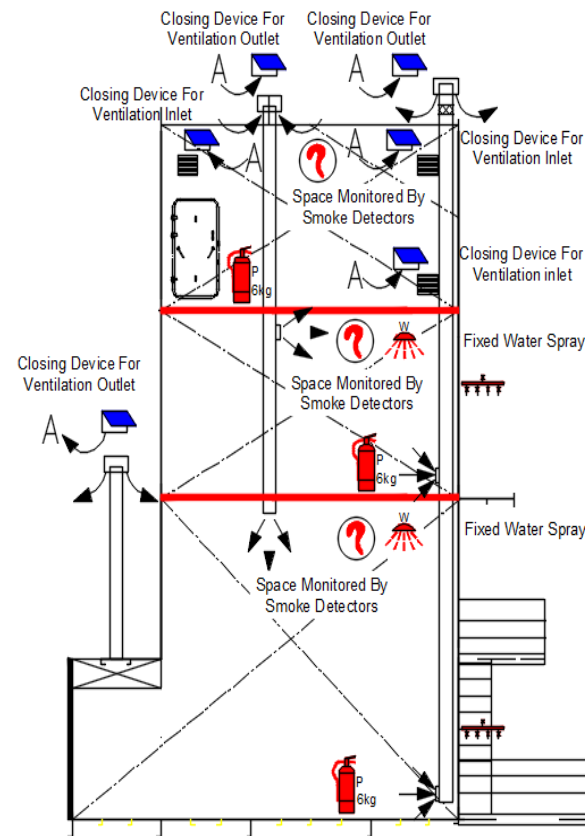
## Identified Hazard



## Control Measure



## Design



## Action Taken

CO<sub>2</sub> & refrigerant detector

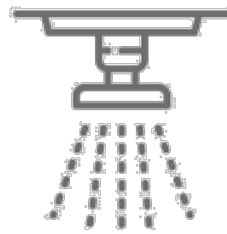
Forced ventilation

## HAZID STUDY - Liquefied CO<sub>2</sub> Tank

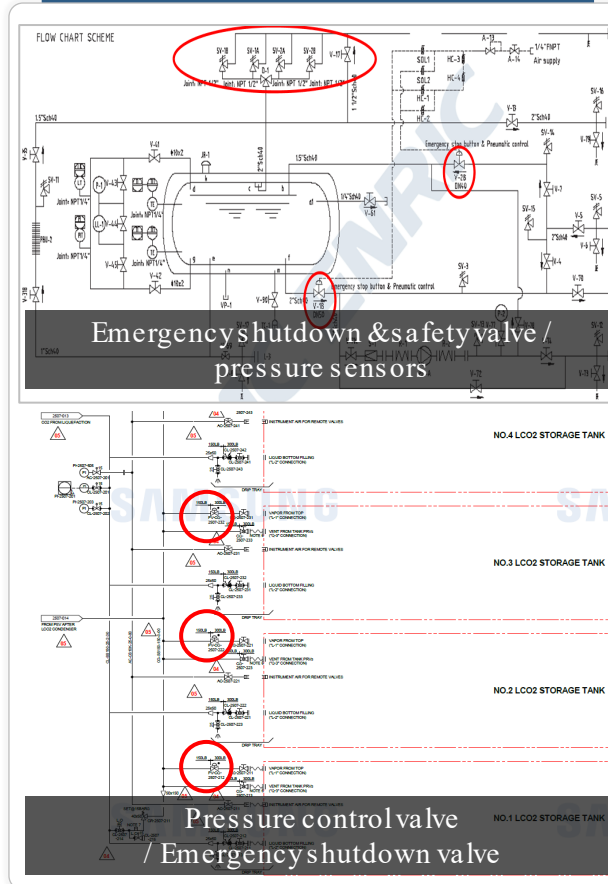
### Identified Hazard



### Control Measure



### Design

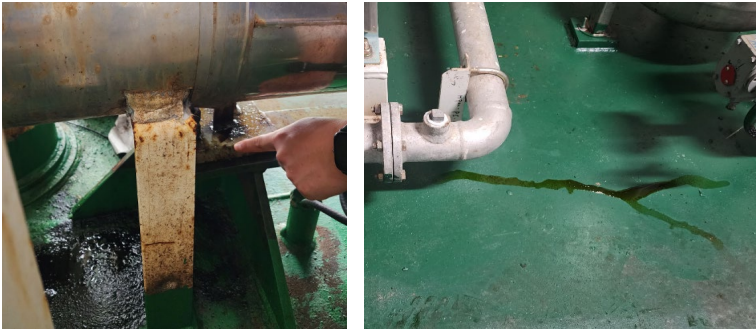


### Action Taken



## Safety issues and Measures 1 Near miss In Operation

### Amine Solvent Leakage

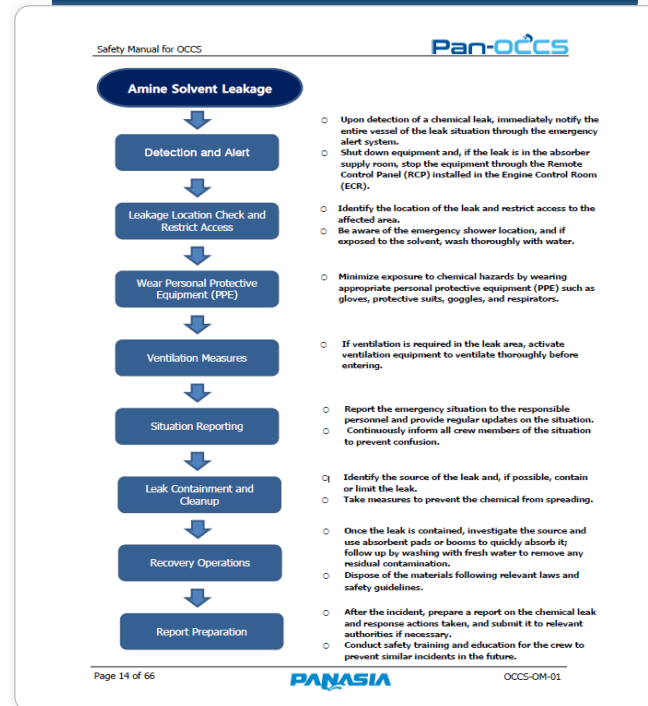


### CO2 Leakage



[ CO2 DETECTOR ]	
CD-004 00.0 %VOL	CD-007 01.2 %VOL
CD-005 00.0 %VOL	CD-008 01.4 %VOL
CD-006 00.0 %VOL	000-C51 00.0 %VOL

### Done Safely in Accordance with the Guidance



### Future Improvements

#### Minimizing Leakage of Solvent & CO<sub>2</sub>



Minimizing flanged connection



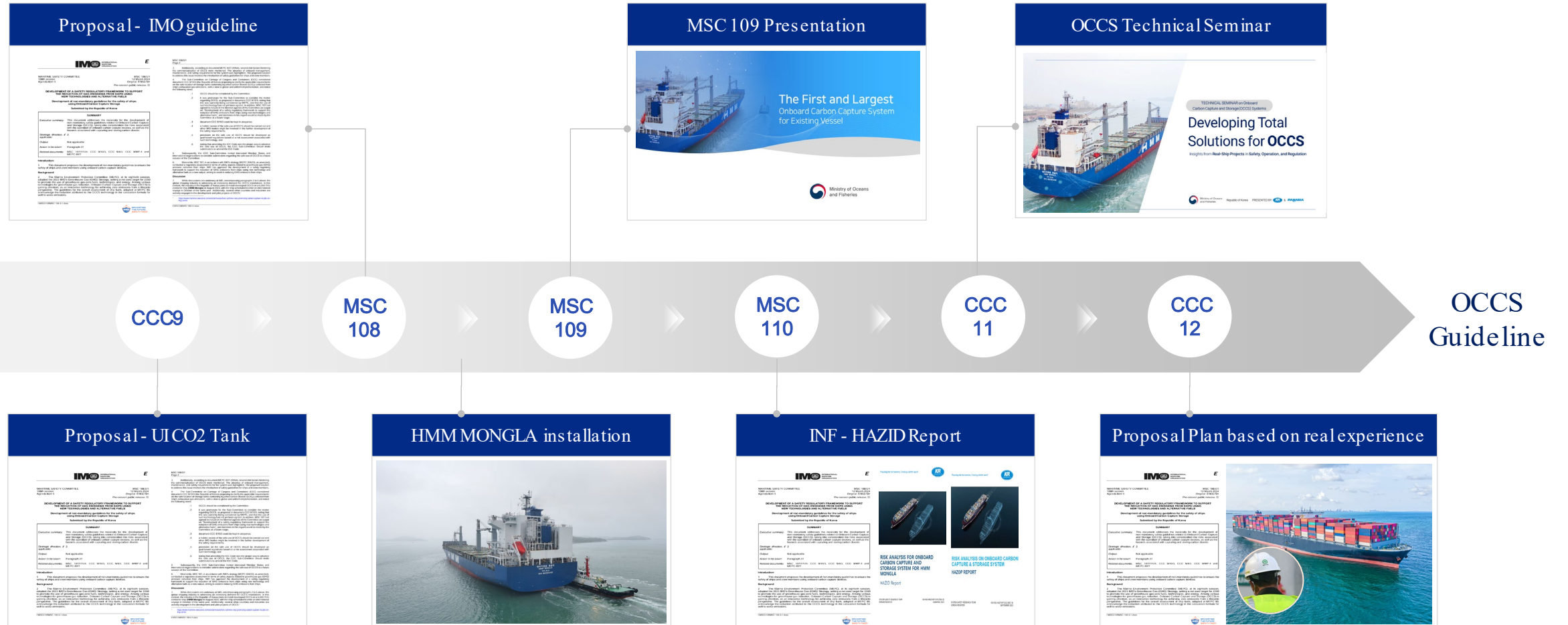
Minimizing instruments



Optimizing piping routes



## ROK's Past Activities and Future Plans at the IMO





# 05

Chapter

## Conclusion

Through this Project, We aim to develop safe and efficient OCCS to achieve decarbonization.

### Safety

- Through HAZID study, Safety Rule developed
- Real time monitoring provide safety.

### Training

- Land base support can make crew less burdened

### Value Chain

- Unloaded CO2 and Utilized it as Methanol

### Efficiency

- High efficiency Carbon Capture with waste heat recovery.

### Space

- Minimize the required space for OCCS.

“ True progress in decarbonization comes from innovation, collaboration, and shared responsibility. ”

# Thanks for your attention



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